

Excess Molar Enthalpies for Binary Mixtures with Trichloroethylene + Alkan-1-ols (C₃–C₈) at 298.15 K

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Excess molar enthalpies H_m^E for trichloroethylene + propan-1-ol, + butan-1-ol, + pentan-1-ol, + hexan-1-ol, + heptan-1-ol, and + octan-1-ol have been measured at 298.15 K with a Parr 1451 solution calorimeter. The H_m^E values are found to be endothermic for all the mixtures rich in alkan-1-ols and become exothermic around 0.15 mole fraction of trichloroethylene. For all the systems, the value of $-H_m^E$ at the minimum increases from propan-1-ol to octan-1-ol. The results are explained in terms of dissociation of the self-associated alkan-1-ol molecules and the formation of aggregates between unlike molecules through Cl \cdots H \cdots O bonding.

Introduction

The magnitude of excess thermodynamic properties such as excess molar enthalpies H_m^E for nonelectrolyte solutions can give a measure of molecular interactions and, hence, can provide information needed to test existing theories of solutions.

This paper forms part of a series on the measurement of thermodynamic properties of nonelectrolyte solutions for binary mixtures with trichloroethylene and tetrachloroethylene as a component in which specific interactions between unlike molecules can occur (Iloukhani et al., 1985a,b; Iloukhani and Rao, 1985). Excess molar enthalpies H_m^E for trichloroethylene + propan-1-ol, + butan-1-ol, + pentan-1-ol, + hexan-1-ol, + heptan-1-ol, and + octan-1-ol at 298.15 K are reported. An inversion of the sign of H_m^E was observed at some mole fraction of trichloroethylene for all binary mixtures. Excess volumes V_m^E for these binary mixtures also showed a similar inversion of sign (Iloukhani et al., 1984).

Experimental Section

Materials. The materials used in this study, their suppliers, and their purities are listed in Table 1. Trichloroethylene was purified by the standard method described by Riddick and Bunger (1970). All alkan-1-ols were purified by the standard method described by Perrin and Armarego (1989).

The purities of the components were checked by measuring their densities and boiling points. The densities were measured at 303.15 K using a bicapillary pycnometer with an accuracy of 5 parts in 10⁵. The boiling points at 101.325 kPa were measured using a Swietoslowski-type ebulliometer which gave an accuracy of ± 0.2 K. Table 1 also gives the density and boiling point measurements for these components together with values obtained from the literature (Riddick and Bunger, 1970; Timmermans, 1962).

Solution Calorimetry. A Parr 1451 solution calorimeter was used. The calorimeter consists of a glass Dewar mixing chamber with a rotating sample cell, a thermistor probe, and a specially designed temperature-measuring bridge, all assembled in a compact cabinet. Temperature changes can be plotted directly using a strip chart recorder and can be read to an accuracy of ± 0.001 K. The two-piece cell serves as both the sample holder and agitator. It is closed with a detachable Teflon disk. The liquid sample can be added to cell from a pipet inserted through the top

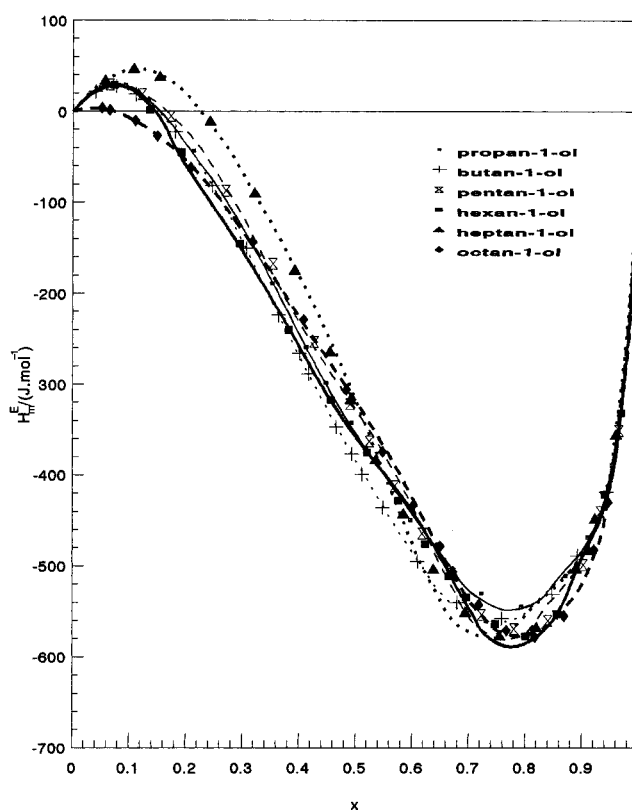


Figure 1. Excess enthalpies for binary mixtures of (x) trichloroethylene + (1 - x) alkan-1-ols at 298.15 K. Continuous curves, (—) propan-1-ol, (---) butan-1-ol, (···) pentan-1-ol, (- · -) hexan-1-ol, (---) heptan-1-ol, and (- - -) octan-1-ol, were calculated from coefficients of eq 1 given in Table 3.

stem. Excellent thermal insulation is provided by the fully silvered glass Dewar which serves as a mixing chamber. Other information regarding the Parr 1451 solution calorimeter has been reported previously (Kumar et al., 1995).

The enthalpy of mixing experiments were conducted in the calorimeter by considering 100 cm³ of one component as solvent and a maximum of 25 cm³ of the other component as solute. In the subsequent runs, 100 cm³ of the previous solution was taken as the solvent and to this pure solute was added. These experiments were continued until the concentration reached 50–60 vol %. This procedure was repeated by interchanging the components. By this method small errors in the earlier part leads to large

Table 1. Source, Purity Grades, Densities ρ , and Boiling Points T_b of the Pure Components at 303.15 K

component	source	purity/(mass %)	$\rho(\text{g}\cdot\text{cm}^{-3})$		T_b/K	
			exptl	lit. ^a	exptl	lit. ^a
trichloroethylene	Merk	99.5%	1.451 31	1.451 4	360.2	360.3
propan-1-ol	Fluka	99%	0.795 91	0.796 00	370.2	370.3
butan-1-ol	Merk	99%	0.802 01	0.802 06	390.7	390.9
pentan-1-ol	Merk	99%	0.807 57	0.807 64	411.0	411.2
hexan-1-ol	Fluka	$\geq 99.5\%$	0.811 93	0.812 01	430.9	431.0
heptan-1-ol	Fluka	$\geq 99\%$	0.821 84 ^b		448.9	449.1
octan-1-ol	Fluka	$\geq 99.5\%$	0.821 87	0.821 92	467.4	467.6

^a Riddick and Bunger 1970; Timmermans, 1962. ^b At 293.15 K.**Table 2. Excess Molar Enthalpies, H_m^E , for Binary Mixtures of Trichloroethylene + Alkan-1-ols at 298.15 K**

x	$H_m^E/(\text{J}\cdot\text{mol}^{-1})$	$\delta H_m^E/(\text{J}\cdot\text{mol}^{-1})$	x	$H_m^E/(\text{J}\cdot\text{mol}^{-1})$	$\delta H_m^E/(\text{J}\cdot\text{mol}^{-1})$	x	$H_m^E/(\text{J}\cdot\text{mol}^{-1})$	$\delta H_m^E/(\text{J}\cdot\text{mol}^{-1})$
$x\text{C}_2\text{Cl}_3\text{H} + (1-x)\text{C}_3\text{H}_7\text{OH}$								
0.0486	26.1	0.1	0.4128	-259.1	1.0	0.7224	-530.1	6.6
0.0926	28.6	0.4	0.4471	-298.3	1.4	0.7938	-544.4	1.2
0.1328	11.9	-0.2	0.4927	-342.5	4.6	0.8719	-510.7	-6.7
0.2130	-43.6	3.8	0.5184	-369.5	1.8	0.9108	-468.1	4.4
0.2861	-117.9	-4.5	0.5972	-449.1	-9.2	0.9533	-388.9	-0.6
0.3526	-189.2	-1.9	0.6573	-493.3	-1.9			
$x\text{C}_2\text{Cl}_3\text{H} + (1-x)\text{C}_4\text{H}_9\text{OH}$								
0.0400	21.5	-0.1	0.4004	-266.1	3.1	0.6797	-540.2	4.9
0.0764	27.3	0.7	0.4168	-288.8	0.4	0.7583	-557.8	4.0
0.1111	18.5	-0.6	0.4658	-347.1	-0.9	0.8474	-531.1	-8.2
0.1809	-22.3	-0.9	0.4933	-376.9	-0.5	0.8928	-488.9	4.6
0.2461	-81.7	-0.1	0.5113	-399.3	-3.8	0.9434	-418.5	-0.6
0.3071	-150.3	1.8	0.5484	-435.7	-2.0			
0.3639	-223.9	-0.4	0.6102	-495.1	-2.0			
$x\text{C}_2\text{Cl}_3\text{H} + (1-x)\text{C}_5\text{H}_{11}\text{OH}$								
0.0652	29.1	0.2	0.4903	-321.6	-2.8	0.7805	-569.5	10.1
0.1224	18.3	-0.3	0.5246	-363.1	-12.3	0.8403	-560.2	-18.0
0.1731	-5.3	1.1	0.5697	-412.1	-14.3	0.9209	-499.0	-9.1
0.2704	-87.2	3.3	0.6183	-464.1	-7.7	0.9331	-440.4	13.1
0.3538	-167.3	-12.6	0.6694	-508.4	11.7	0.9654	-351.2	-2.6
0.4268	-253.2	-6.3	0.7233	-553.4	16.6			
$x\text{C}_2\text{Cl}_3\text{H} + (1-x)\text{C}_6\text{H}_{13}\text{OH}$								
0.0730	28.6	0.6	0.5203	-375.3	-0.6	0.8004	-577.1	8.1
0.1361	1.4	-4.5	0.5757	-428.2	-9.9	0.8558	-552.6	-15.0
0.1911	-45.2	6.4	0.6236	-476.1	-13.6	0.9130	-483.5	-9.1
0.2947	-145.3	3.0	0.6653	-511.1	-3.7	0.9403	-421.3	12.7
0.3818	-240.1	-2.3	0.6959	-534.2	7.0	0.9692	-332.2	-2.6
0.4563	-317.2	1.2	0.7471	-563.9	19.6			
$x\text{C}_2\text{Cl}_3\text{H} + (1-x)\text{C}_7\text{H}_{15}\text{OH}$								
0.0569	34.5	1.1	0.4551	-263.6	-11.8	0.7546	-576.3	-1.4
0.1076	47.4	1.9	0.4913	-316.6	-12.6	0.8197	-566.8	-25.5
0.1532	38.5	-1.6	0.5364	-382.3	-8.1	0.8894	-502.0	-4.2
0.2425	-10.1	4.0	0.5850	-441.9	9.0	0.9234	-447.3	14.2
0.3213	-89.2	2.2	0.6375	-503.0	19.8	0.9602	-354.8	-3.3
0.3922	-173.7	-2.5	0.6940	-550.2	20.0			
$x\text{C}_2\text{Cl}_3\text{H} + (1-x)\text{C}_8\text{H}_{17}\text{OH}$								
0.0513	3.7	0.1	0.4080	-229.1	4.2	0.7186	-542.3	8.7
0.0652	1.3	-0.2	0.4839	-306.0	-2.7	0.7670	-570.0	4.2
0.1104	-10.3	0.6	0.5479	-374.4	-8.4	0.8171	-578.2	-5.3
0.1492	-27.3	-0.4	0.6025	-433.3	-6.2	0.8685	-554.9	-7.3
0.2082	-61.9	-1.5	0.6494	-478.1	4.2	0.9212	-482.6	7.3
0.3176	-143.5	4.2	0.6719	-506.3	1.2	0.9460	-429.8	-2.8

Table 3. Values of the Adjustable Coefficients, A_i , in Eq 1 and the Standard Deviation, $\sigma(H_m^E)$, in Eq 2 for Trichloroethylene + Alkan-1-ols at 298.15 K

A_i, σ	$\text{C}_2\text{Cl}_3\text{H} +$					
	$\text{C}_3\text{H}_7\text{OH}$	$\text{C}_4\text{H}_9\text{OH}$	$\text{C}_5\text{H}_{11}\text{OH}$	$\text{C}_6\text{H}_{13}\text{OH}$	$\text{C}_7\text{H}_{15}\text{OH}$	$\text{C}_8\text{H}_{17}\text{OH}$
A_1	-1416.8	-1534.4	-1311.0	-1432.9	-1268.8	-1273.6
A_2	1907.9	2133.3	1839.2	1674.0	3054.3	1899.4
A_3	-121.1	-840.3	-1899.7		-2643.4	-2024.3
A_4	4120.3	2965.8	7261.8	5836.1		4528.4
A_5	-6886.2			-14532.5	8105.0	
A_6	-10105.7	-7936.9	-18921.5	-12718.6	-3427.1	-10388.7
A_7	17582.9	2810.5	7307.9	39810.6	-10792.7	3572.6
A_8	11984.3	10542.3	18528.1	12963.4	7858.5	11512.4
A_9	-16813.5	-7438.6	-11836.7	-33395.8		-7280.3
σ	5.7	3.9	13.1	12.3	14.7	6.4

errors in later experiments. Because of the limitations of the calorimeter, one is forced to adopt this method to cover the entire concentration range.

Initially, the calorimeter was calibrated with 0.5 g of (hydroxymethyl)aminomethane dissolved in 0.1 mol·dm⁻³ hydrochloric acid solution to evolve 245.52 J·g⁻¹ at 298.15 K to determine the calorimeter equivalent. The performance and reliability of the solution calorimeter were checked by making measurements on both endothermic and exothermic systems: C₆H₆ + CCl₄ and C₆H₅Cl + C₆H₅-CH₃. The excess enthalpies H_m^E agreed with the literature values to within 2% (Nicolaides and Eckert, 1978; Tanaka and Benson, 1976).

Results and Discussion

The measured molar excess enthalpies H_m^E of trichloroethylene + propan-1-ol, + butan-1-ol, + pentan-1-ol, + hexan-1-ol, + heptan-1-ol, and + octan-1-ol at 298.15 K are listed in Table 2, together with the deviations $\delta(H_m^E)$ and shown graphically in Figure 1. The results were fitted to the Redlich–Kister (R–K) polynomial

$$H_m^E/(\text{J}\cdot\text{mol}^{-1}) = x(1-x)\sum A_i(1-2x)^{i-1} \quad (1)$$

where A_i are the coefficients for the binary systems. They are presented in Table 3 together with the standard deviation $\sigma(H_m^E)$ which is evaluated from the equation

$$\sigma(H_m^E) = |\phi/(n-p)|^{0.5} \quad (2)$$

where n is the number of the experimental points and p the number of adjustable parameters A_i . ϕ is the objective function defined as

$$\phi = \sum \delta^2(H_m^E) \quad (3)$$

where $\delta(H_m^E) = H_{m,\text{expt}}^E - H_{m,\text{calcd}}^E$.

The excess enthalpies varies very little with the chain length of the alkan-1-ols, and the minimum value of H_m^E decreases from octan-1-ol to propan-1-ol.

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